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1,53 10,79 %

Введение

[1–4]

[5–8]

[9–12].

[3],

20–30%,

6–8% [13].

[14]

[15].

[1, 4, 16–19].

[20]

[20]

[11, 12, 17, 21,

22].

30

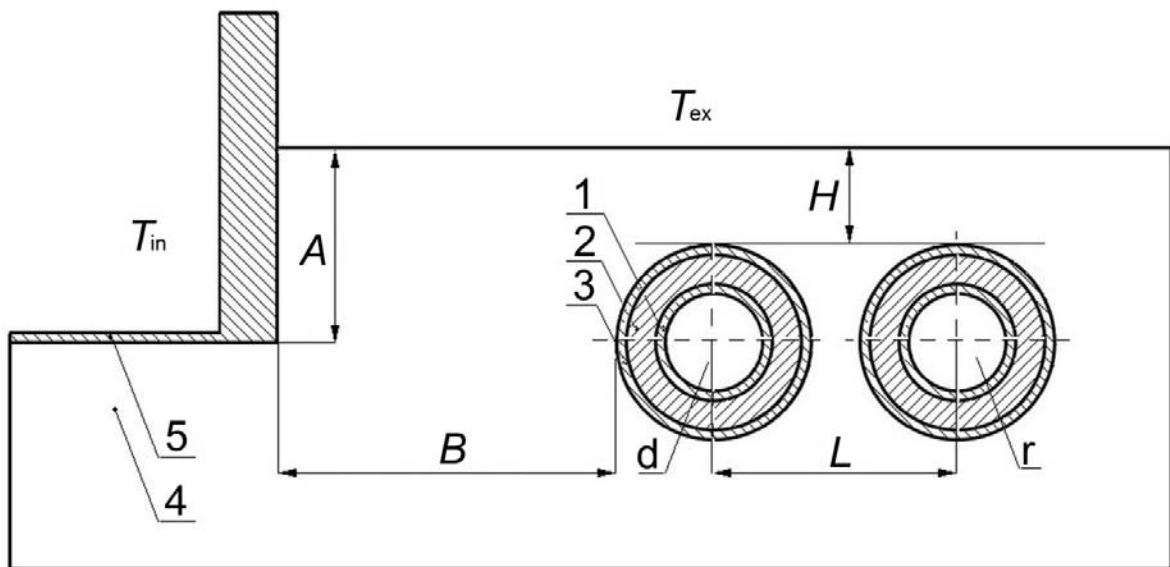
[23]



),

Постановка задачи

[24].



1 - ; 2 - ; 3 - ;
 4 - ; 5 - ;
 d, r - ;
 L - ; A - ; B - ;
 H - ;

« (1) - »

(1)

[21, 22].

1. (1).
- 2.
- 3.
- 4.

Математическая модель

[11, 12, 21, 22, 25–27]

⋮

$$\nabla^2 T_{d,p} = 0; \tag{1}$$

$$\nabla^2 T_{r,p} = 0; \tag{2}$$

$$\nabla^2 T_{d,i} = 0; \tag{3}$$

$$\nabla^2 T_{r,i} = 0; \tag{4}$$

$$\nabla^2 T_{d,h} = 0; \tag{5}$$

$$\nabla^2 T_{r,h} = 0; \tag{6}$$

$$\nabla^2 T_g = 0; \tag{7}$$

$$\nabla^2 T_f = 0. \tag{8}$$

,

:

$$T_{d,p,1} = T_d = const; \tag{9}$$

$$T_{r,p,1} = T_r = const. \tag{10}$$

:

$$\lambda_p grad(T_{d,p,2}) = \lambda_i grad(T_{d,i,2}); T_{d,p,2} = T_{d,i,2}, \tag{11}$$

$$\lambda_p grad(T_{r,p,2}) = \lambda_i grad(T_{r,i,2}); T_{r,p,2} = T_{r,i,2}, \tag{12}$$

$$\lambda_i grad(T_{d,i,3}) = \lambda_h grad(T_{d,h,3}); T_{d,i,3} = T_{d,h,3}, \tag{13}$$

$$\lambda_i grad(T_{r,i,3}) = \lambda_h grad(T_{r,h,3}); T_{r,i,3} = T_{r,h,3}, \tag{14}$$

$$\lambda_h grad(T_{d,h,4}) = \lambda_g grad(T_{d,g,4}); T_{d,h,4} = T_{d,g,4}, \tag{15}$$

$$\lambda_h grad(T_{r,h,4}) = \lambda_g grad(T_{r,g,4}); T_{r,h,4} = T_{r,g,4}, \tag{16}$$

$$\lambda_g grad(T_{g,5}) = \lambda_f grad(T_{f,5}); T_{g,5} = T_{f,5}. \tag{17}$$

« — », « —

» « —

»

:

$$-\lambda_g grad(T_{g,6}) = \alpha_6(T_{g,6} - T_{ex}); \tag{18}$$

$$-\lambda_f grad(T_{f,7}) = \alpha_7(T_{f,7} - T_{in}); \tag{19}$$

$$-\lambda_f grad(T_{f,8}) = \alpha_8(T_{f,8} - T_{in}); \tag{20}$$

$$-\lambda_f grad(T_{f,9}) = \alpha_9(T_{f,9} - T_{ex}). \tag{21}$$

$$(1) \quad \dots \dots \dots$$

$$\text{grad}(T_g) = 0, x \rightarrow \pm\infty; y \rightarrow -\infty; \quad (22)$$

$$\text{grad}(T_f) = 0, x \rightarrow -\infty; y \rightarrow +\infty. \quad (23)$$

Обозначения: T – температура; λ – коэффициент теплопроводности; ρ – плотность; c – удельная теплоемкость; μ – динамическая вязкость; ν – кинематическая вязкость.

Индексы: d – диаметр; r – радиус; p – пористость; i – индекс; h – толщина; g – индекс; f – индекс; in – внутренний; ex – внешний; 1 – индекс; 2–9 – индекс.

Метод решения и исходные данные

(1)–(23)

COMSOL Multiphysics

General Heat Transfer [28], [29], 30].

36015 18038 Mesh COMSOL Multiphysics [28].

(22), (23), 7 16

0,5%. 0,377

10 (0,006), 0,0553 [24], $H = 1,5 \frac{B}{A}$ [24]. 1).

$L = 0,65$, 2 5

(1), $A = 2$, $T_d = T_r$

[31], 95/70 °

$T_{ex} = 264,35$ [32], $T_{in} = 275,15$, 293,15 [33]

$\tau = 8,7$ l , $\delta = 4,5$ l , $\delta = 15$ l , $\rho = 23$ l .

(ρ) [34] (λ), (C)

Таблица 1. Теплофизические характеристики материалов

| | | | | | |
|-----------------------------|------|-------|------|------|------|
| λ , $W/(m \cdot K)$ | 0,33 | 0,033 | 50,2 | 1,5 | 1,54 |
| c , $J/(kg \cdot K)$ | 2200 | 1470 | 462 | 1150 | 887 |
| ρ , kg/m^3 | 920 | 50 | 7700 | 1960 | 2200 |

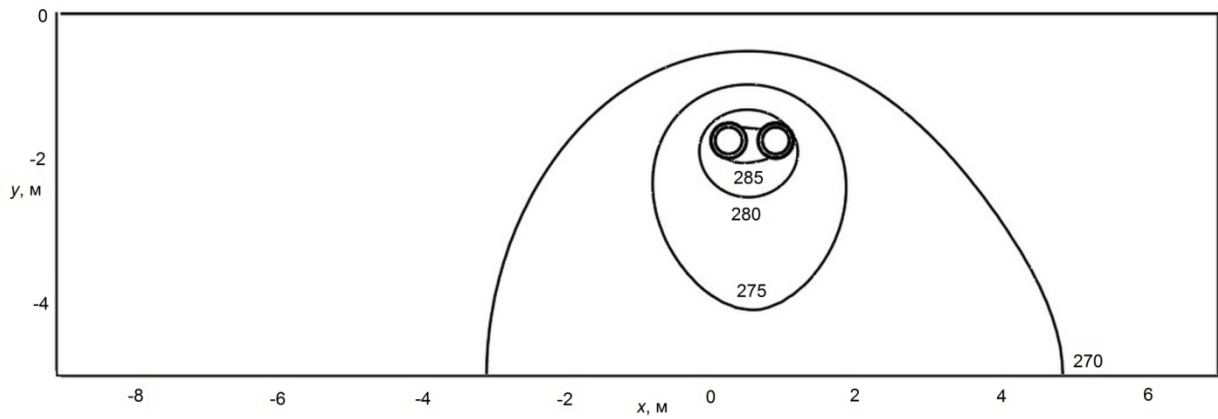
Результаты численного моделирования

2-4. e 2
 [35, 36].
 0,5 %
 2 (q₂ 1),
 q₁ [20, 31]. q

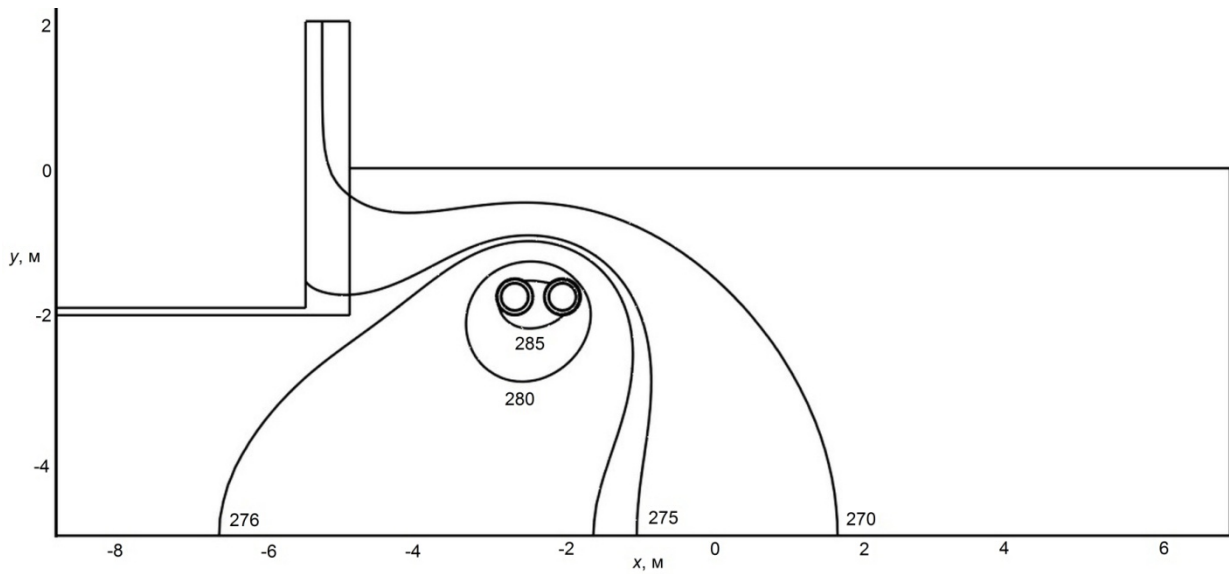
Таблица 2. Результаты численного моделирования (q₁ = 74,74 Вт/м; q_{норм} = 99,50 Вт/м)

| B, | T _{in} , | q ₂ , l | $\delta_1 = \frac{q_1 - q_2}{q_1} 100\%$ | $\delta_2 = \frac{q_{норм} - q_2}{q_{норм}} 100\%$ |
|----|-------------------|--------------------|--|--|
| 5 | 275,15 | 73,36 | 1,85 | 26,27 |
| | 293,15 | 70,96 | 5,06 | 28,68 |
| 2 | 275,15 | 72,17 | 3,44 | 27,47 |
| | 293,15 | 66,68 | 10,79 | 32,99 |

2, q₂
 5 2
 T_{in} = 275,15 6,03 % 1,62 %
 T_{in} = 293,15
 275,15 293,15
 3,27 % 7,61 % B = 2 B = 5
 q₁ q₂ (2)
 δ₁ = 1,53 % δ₁ = 10,79 % T_{in} B.
 [20, 31], q₂ q [20, 31]
 δ₂ 26,27 32,99 %.
 2-4
 (. 2) (. 3, 4).

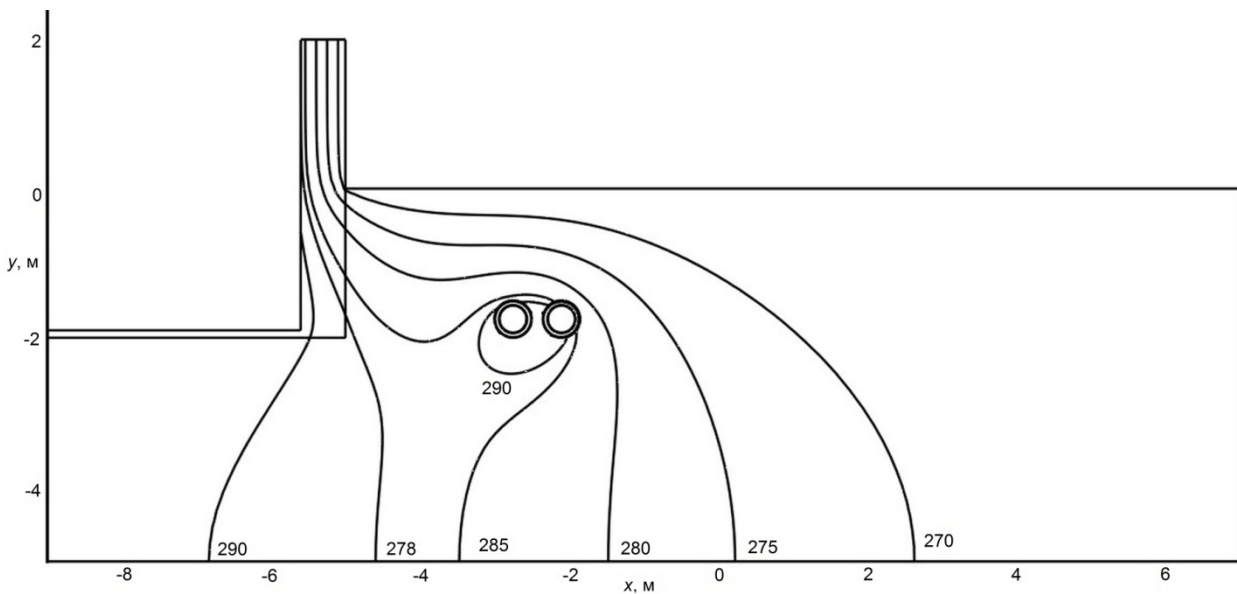


2.



3.

$(B = 2, T_{in} = 275,15)$



4.

$(B = 2, T_{in} = 293,15)$

(. 2–4)

[21, 22]

[35, 36]

[35, 36].

(' 2)

[20, 31]

[1–12, 21–23, 35–38]

Заклучение

10,79 %

1,53

[20, 31]

[20, 31]

33 %.

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Numerical analysis of the impact of engineering constructions on heat loss of channel-free heat pipelines

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Key words

mathematical modeling; channel-free heat pipelines; heat loss; engineering constructions

Abstract

The work shows the results of mathematical modelling of thermal conditions for channel-free heating network laid in the areas of influence of engineering constructions, as well as the results of numerical analysis of heat losses in the objects under examination.

The regularities of heat transfer in the system concerned and the factors influencing intensification of heat losses are revealed. The heat losses in channel-free pipes laid in the areas of engineering constructions influence have been found to decrease in the range from 1.53 to 10.79%, depending on the temperature inside any given engineering structure and geometric characteristics of the system under examination.

It is demonstrated that the standard method of heat loss calculation for channel-free heating pipes overestimates values of heat loss.

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